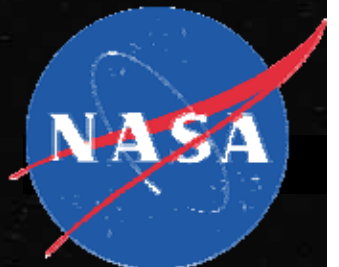




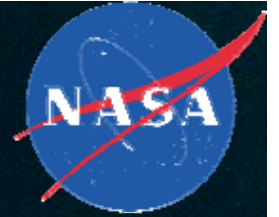
# IN-SITU PRODUCTION OF OXYGEN THROUGH LUNAR REGOLITH PYROLYSIS

Eric Cardiff, Ian Banks  
NASA GSFC

Tamela Maciel  
University of Oregon



# ISRU Techniques



## Solid Gas Interaction:

- Reduction mechanism ( $H_2$ , C, CO,  $CH_4$ ,  $H_2S$ ,  $Cl_2$ )
- Fluorination replacement
- Carbo-chlorination.

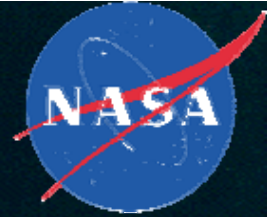
## Molten Processes:

- Molten Electrolysis (fluxed melting)
- Molten reduction (carbothermal, Li reduction)
- Oxygen beneficiation (oxidation and complete reduction)

## Pyrolysis:

- Vacuum or Vapor phase
- Plasma (10,000 C) separation, or reduction

## Acid Dissolution

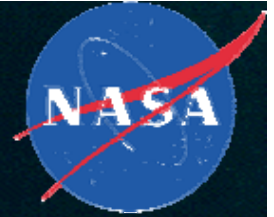


# Vacuum Pyrolysis

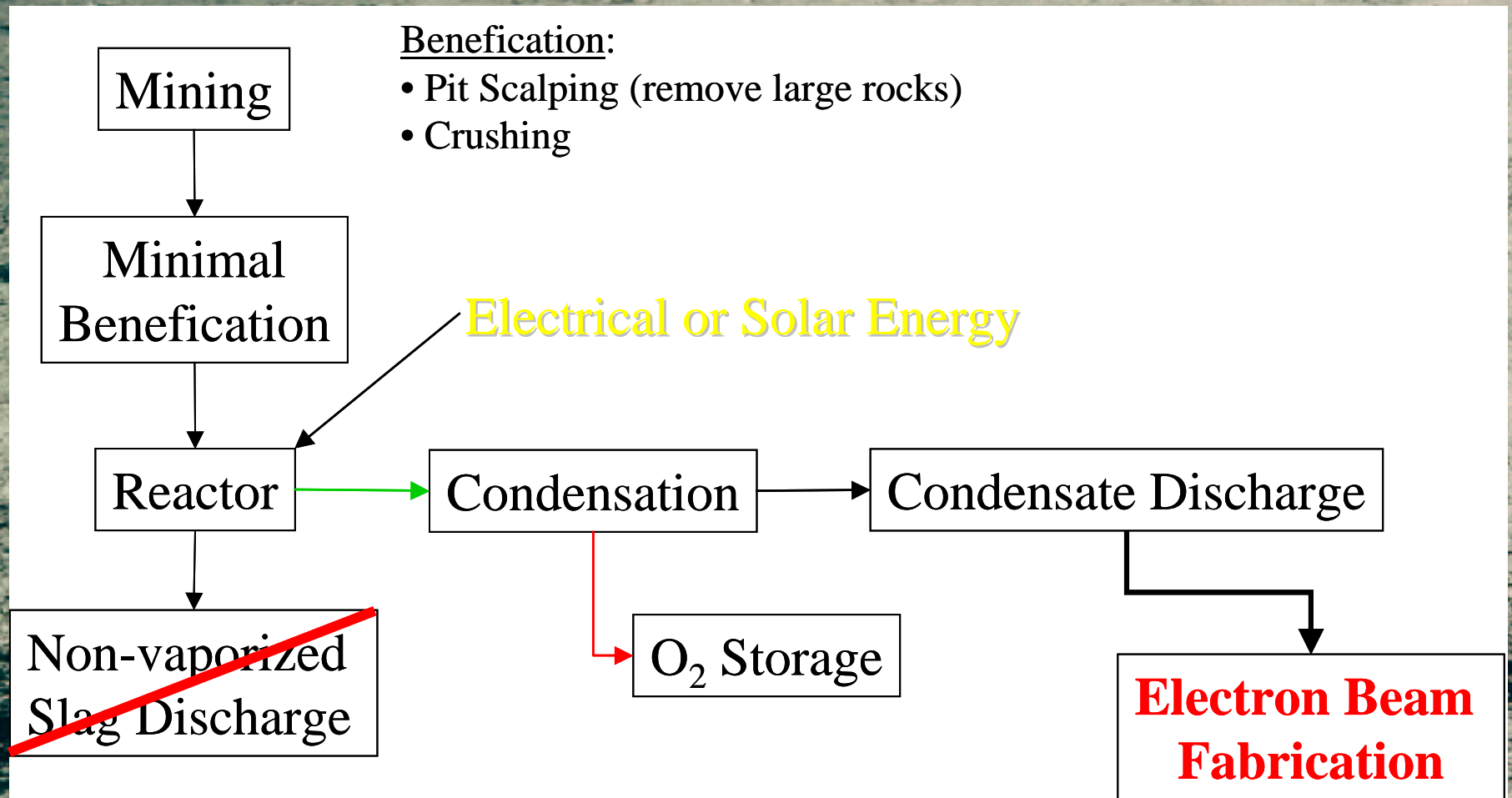
- Vacuum pyrolysis is based on the vaporization reaction of metal oxides that simultaneously reduces the oxide and produces O<sub>2</sub>.



- The reduced oxide can be condensed out of the low-pressure gas as the gasses cool.
- Vacuum pyrolysis has a high potential efficiency (up to 0.2 g/g).
- The process requires no imported chemicals/consumables.
- Can produce metallic byproducts from the condensation.

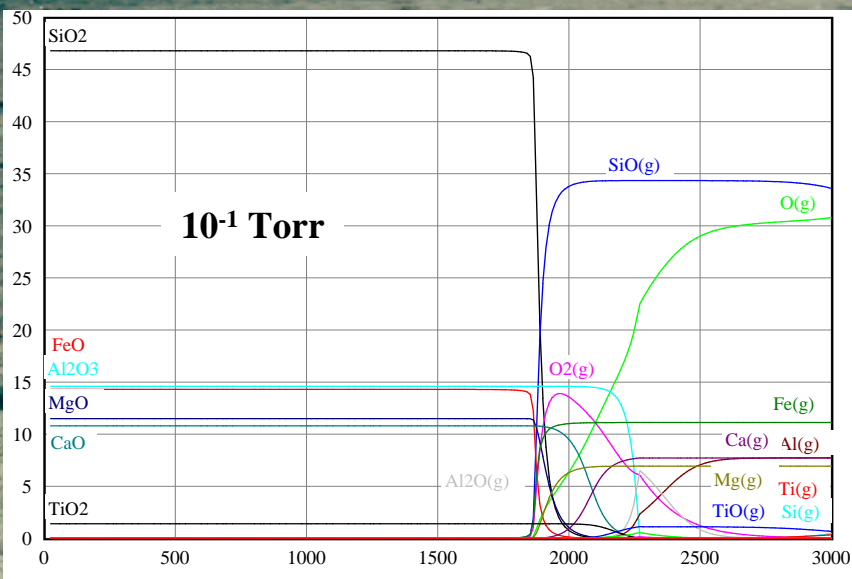


# Process Diagram

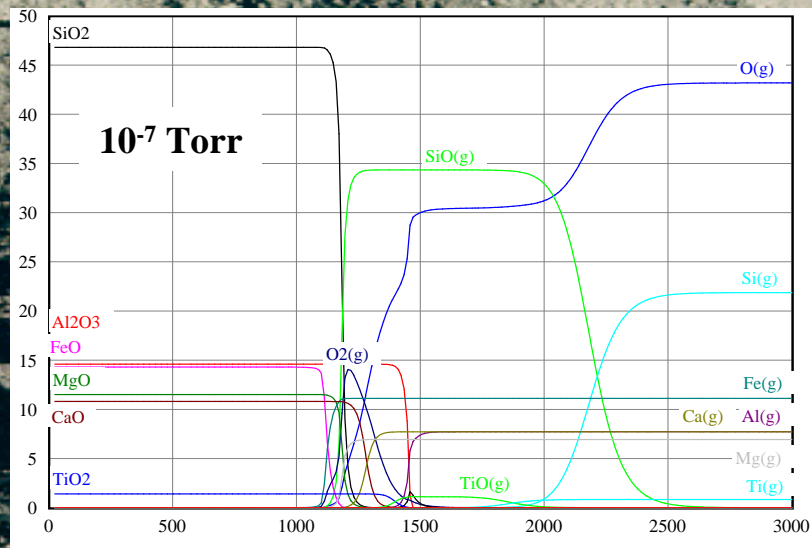




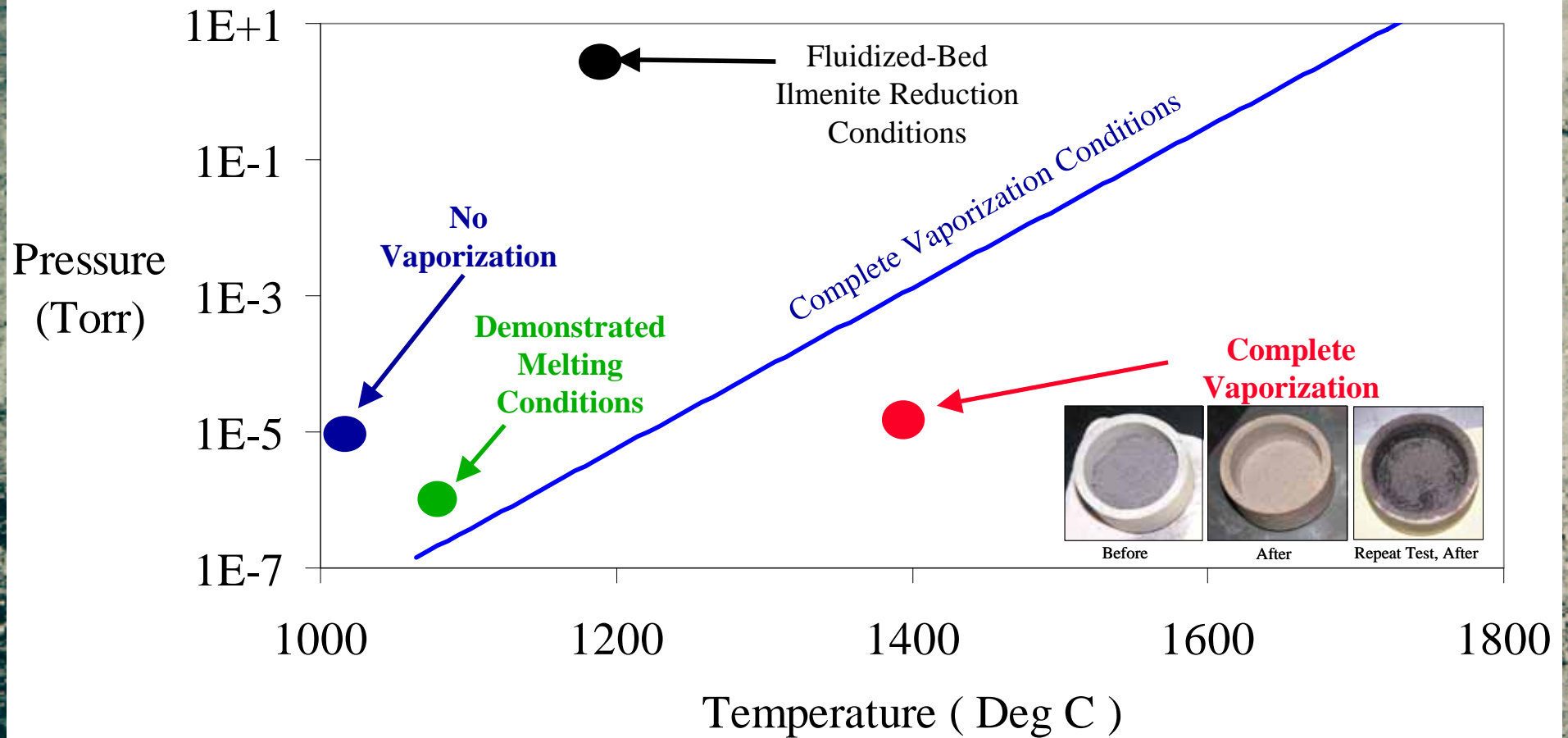
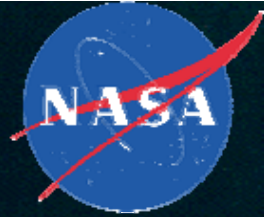
# Pressure Effects



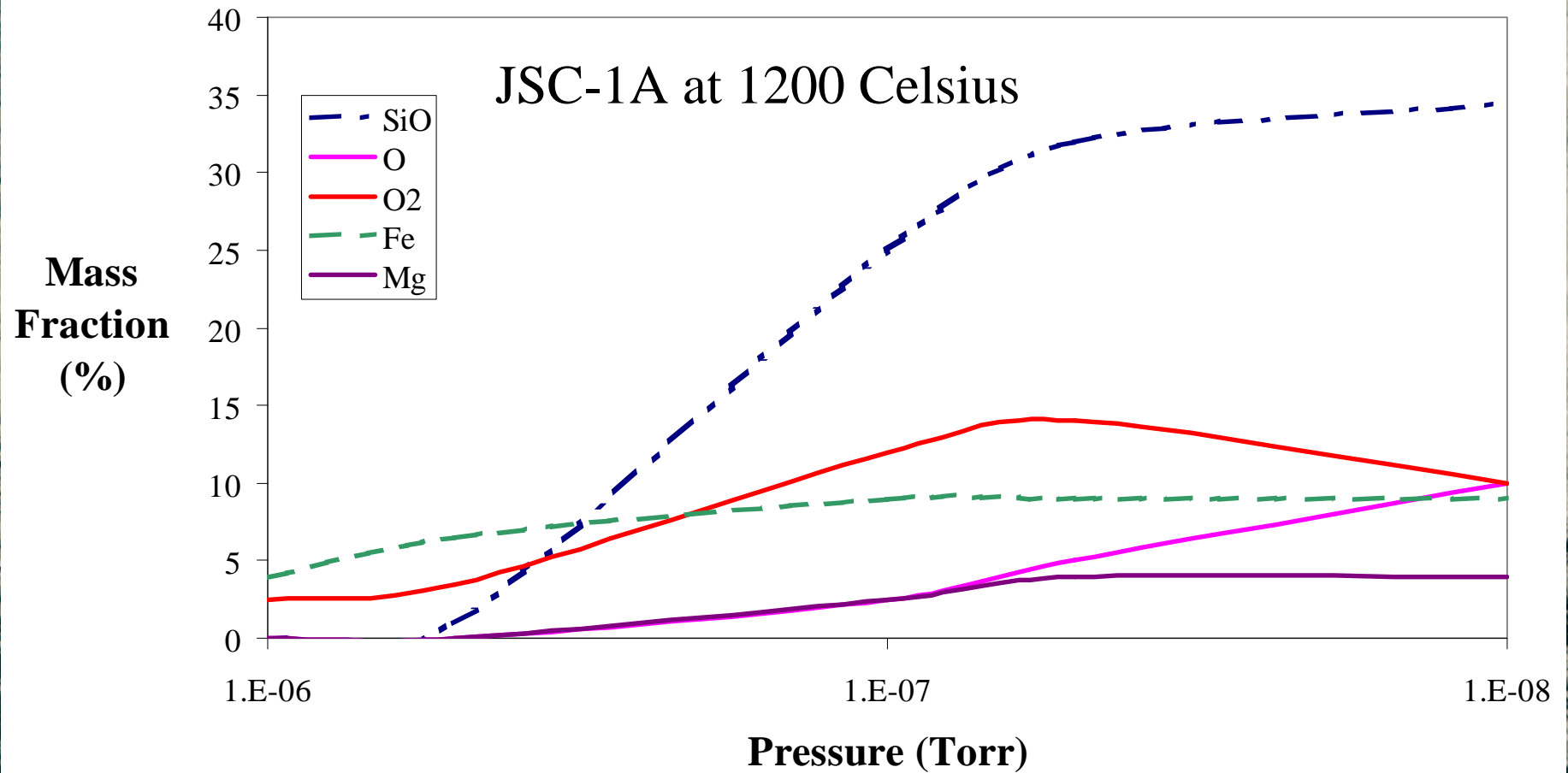
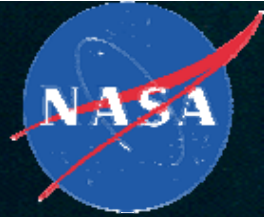
**Reduced pressure  
Significantly reduces  
the vaporization  
temperature of MLS-1.**



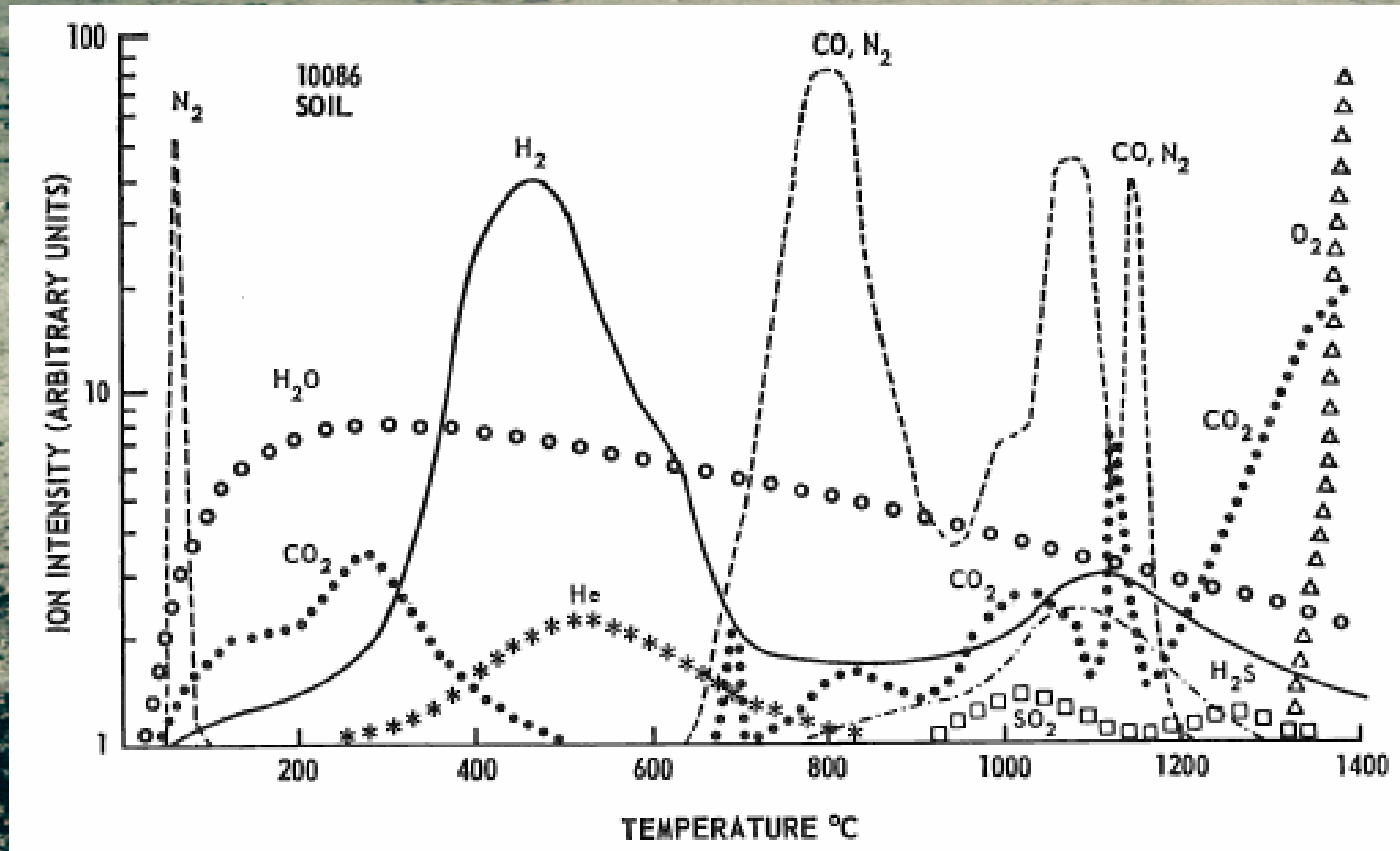
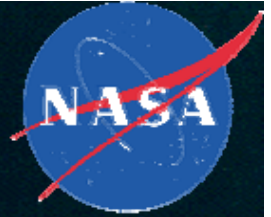
# Operating Conditions

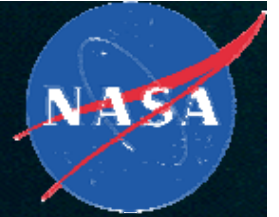


# Expected Yields



# Vacuum Pyrolysis of Apollo 11 Sample 10086

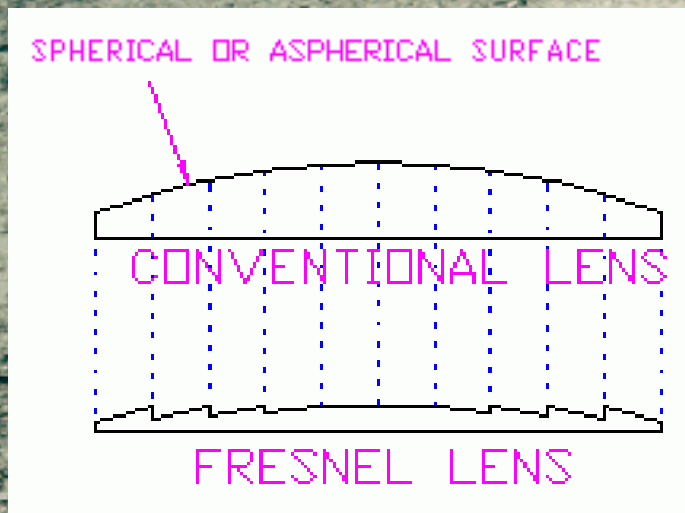
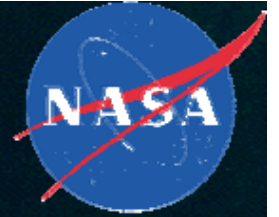


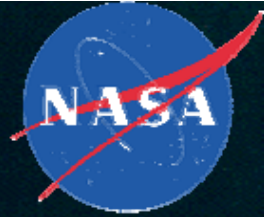


# Systems Designed

	Solar Prototype	Solar Reflector	VAPoR	High Temperature	2 <sup>nd</sup> Generation
Power (W)	650	10,000	60	500	210
Max Temp (C)	1870	1500+	1300	1100	1300
Chamber Mass (kg)	35	300	18	12	30
Sample Size (g)	20	2000	0.15	20	20

# Prototype System

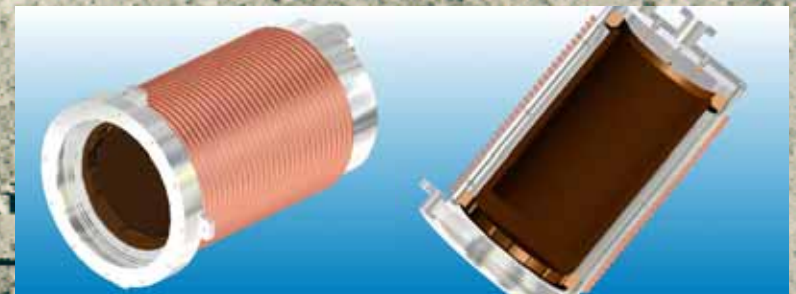




# Indirect Solar



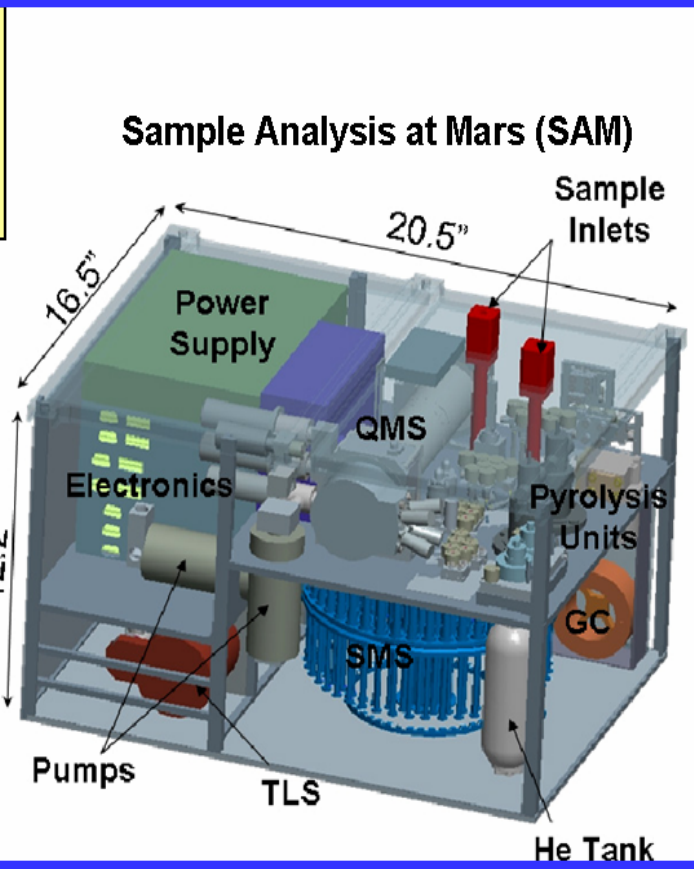
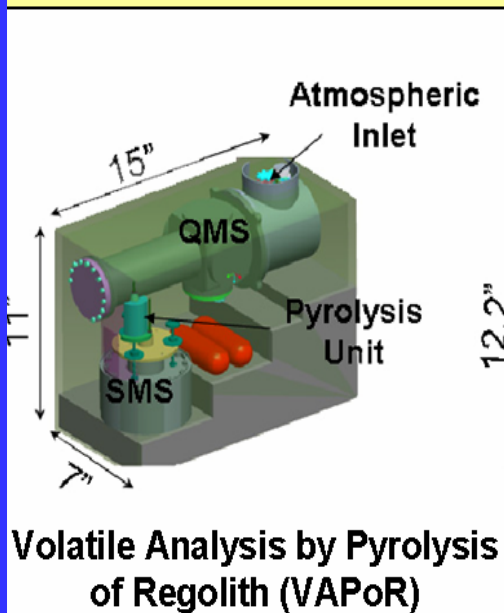
**3.8 m solar reflector**



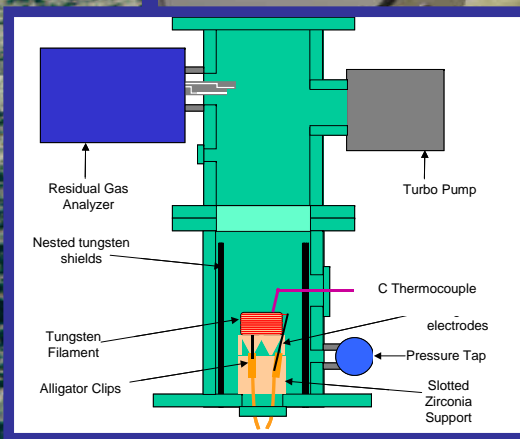
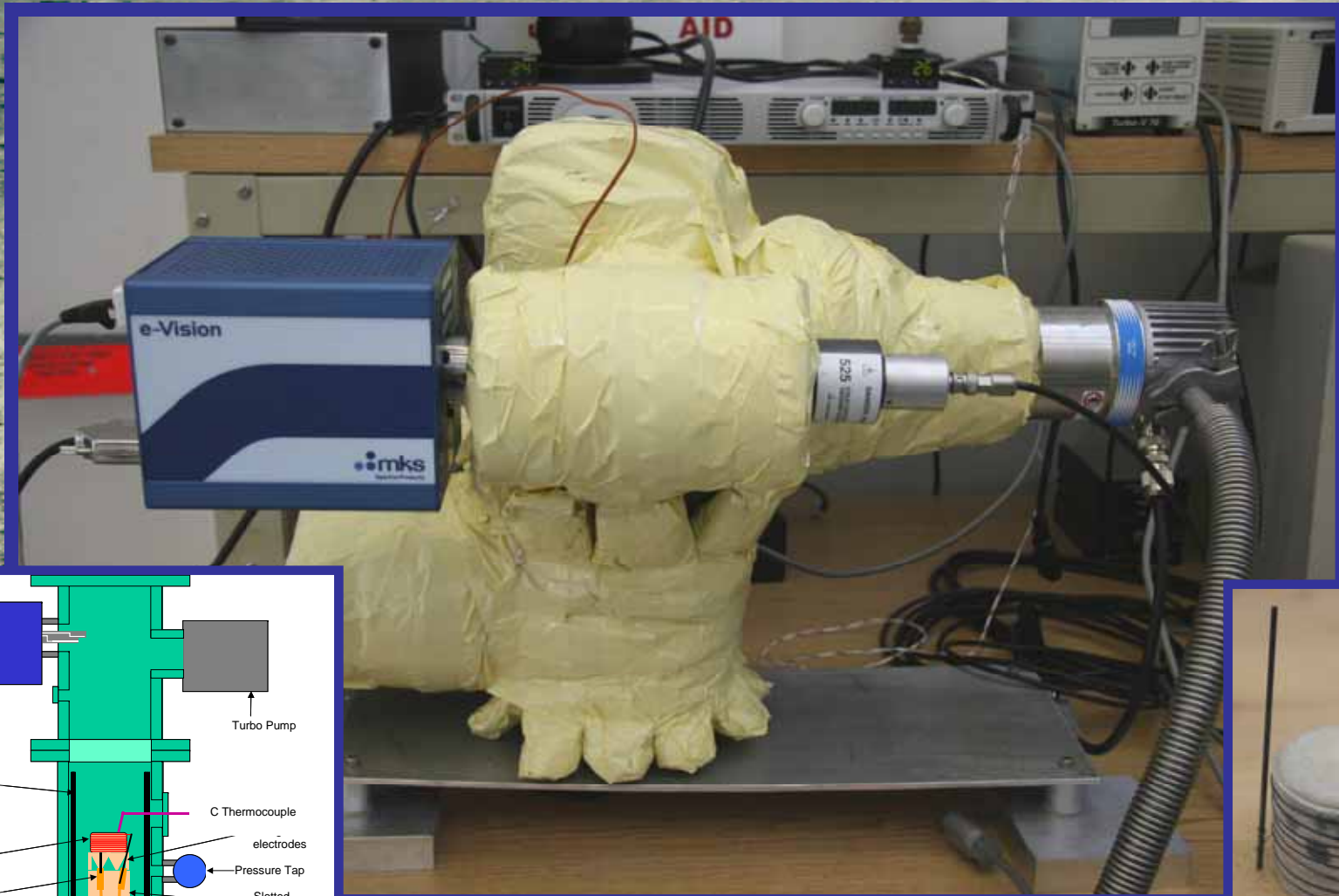
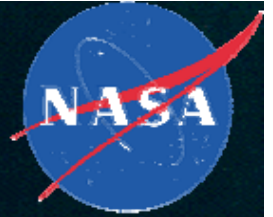
# VAPoR

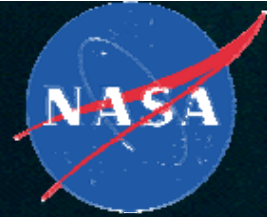


	<b>VAPoR</b>	<b>SAM</b>
Mass:	7-15 kg	40 kg
Power:	20-25 W	60-80 W
Data rate:	1 kbps	<100 kbps
Volume:	19 dm <sup>3</sup>	68 dm <sup>3</sup>



# High Temperature Chamber



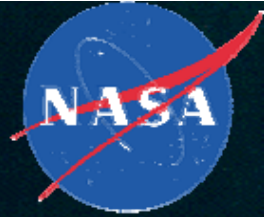


# Chamber Improvements

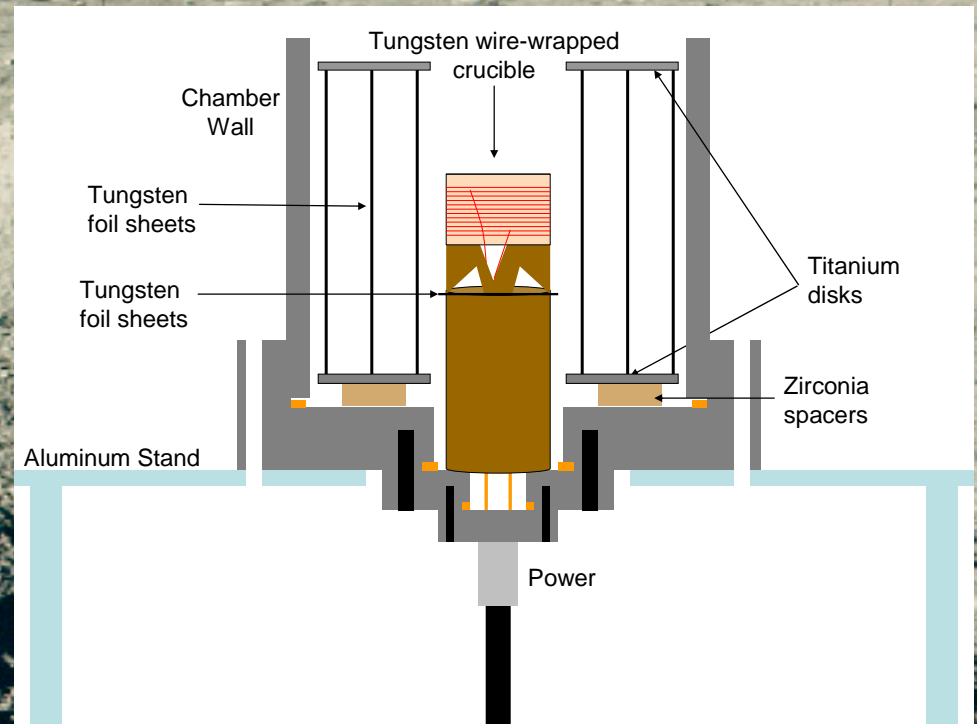
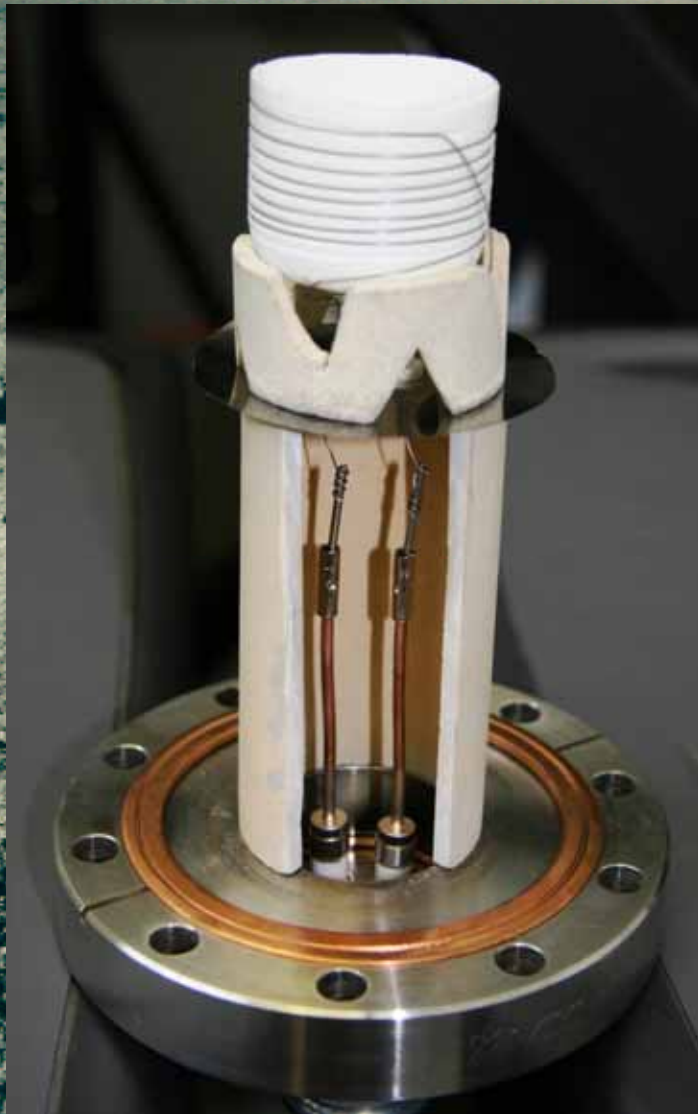
- Improved modular shields
- Reduced thermal contacts
- Higher thermal limit materials
- Improved power feed system
- Improved instrumentation
- Increased the maximum power capability

# 2<sup>nd</sup> Generation Chamber

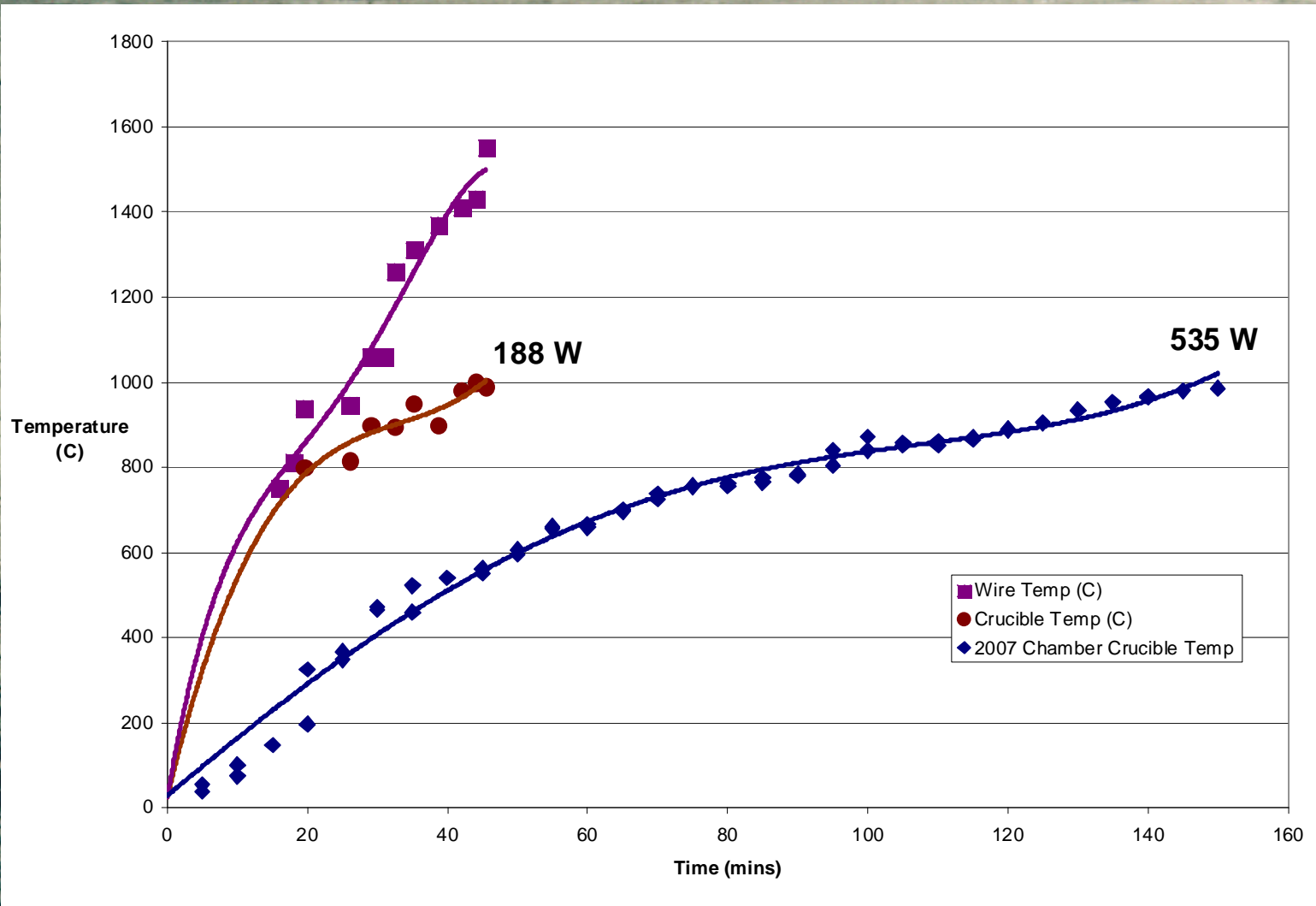
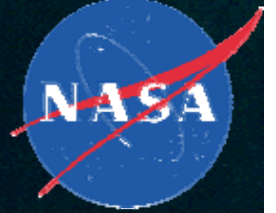




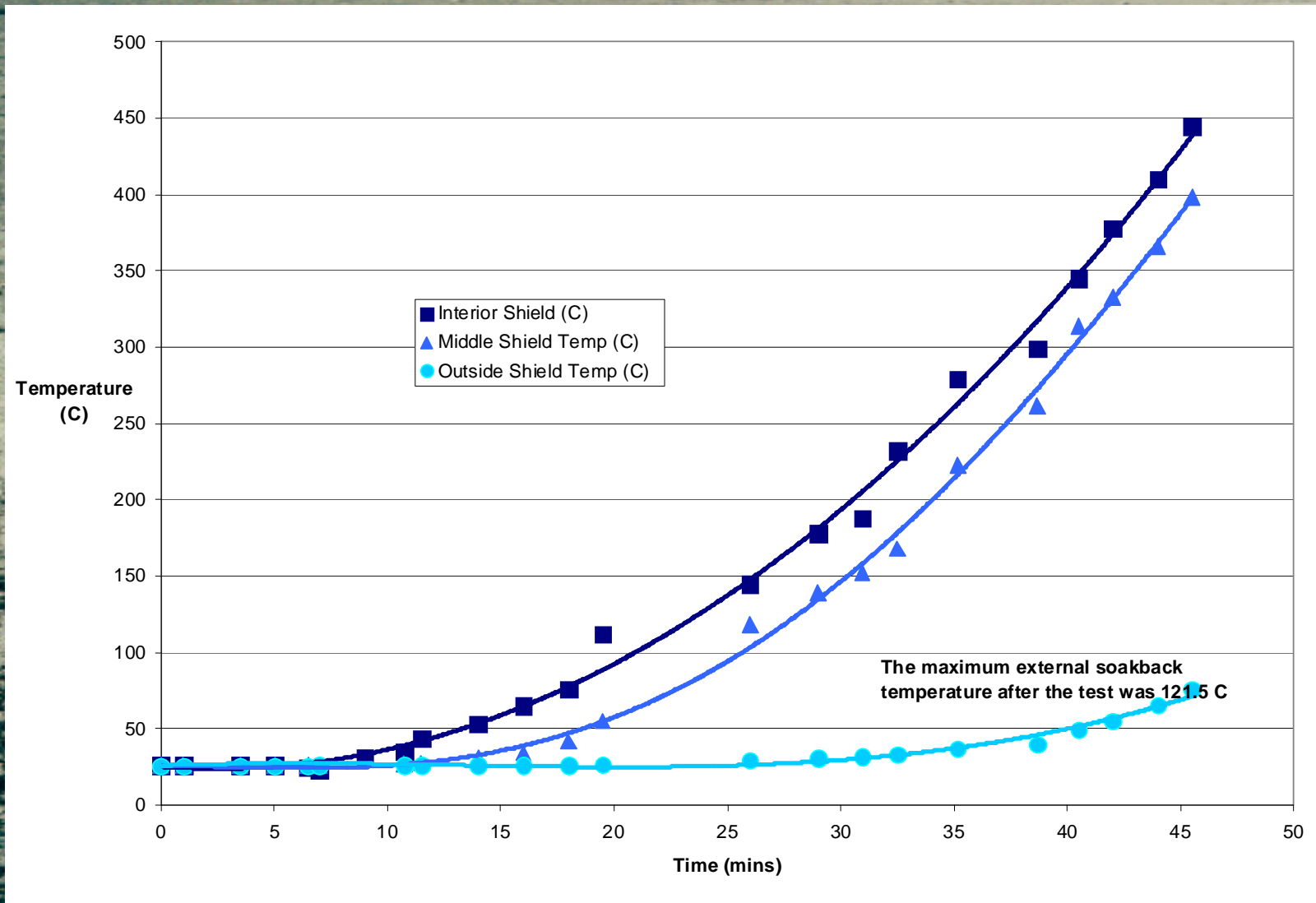
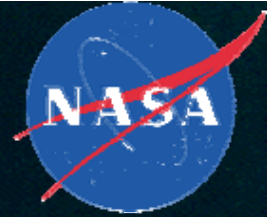
# Chamber Details

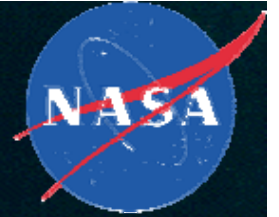


# Heating Profiles



# Shield Temperatures

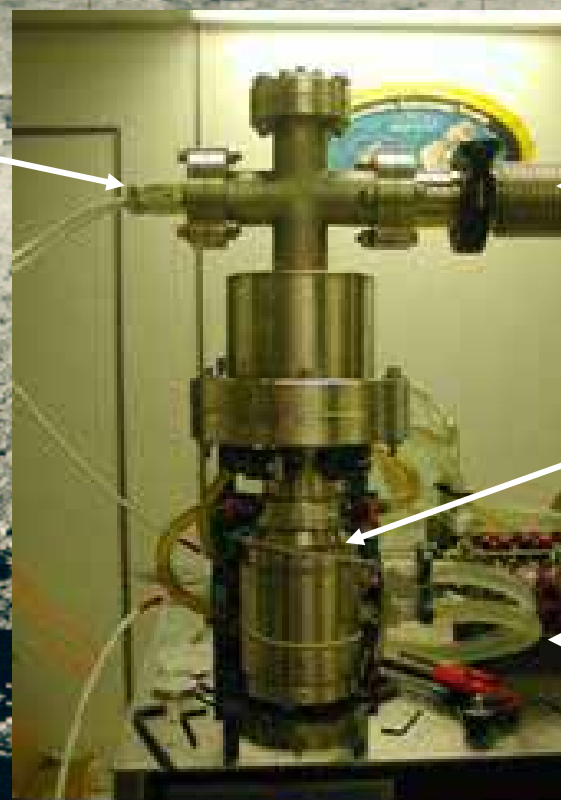
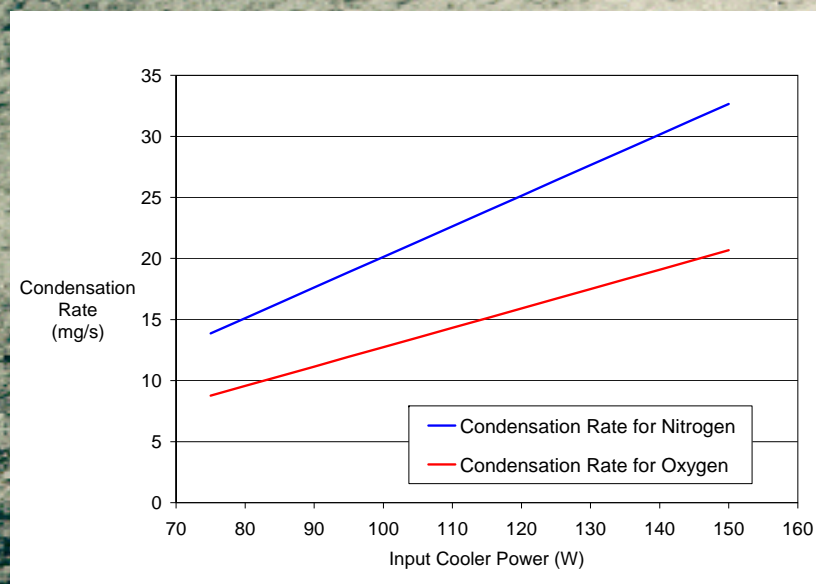




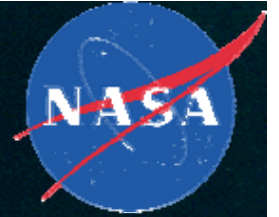
# Scaling Calculations

- We calculated an effective thermal capacitance of the crucible + regolith:  
0.41 W.hr/kg.C
- Scaling assumptions:
  - 1500 C
  - 2 hour process time
  - Sample mass of 12 kg
  - 50% on-time
- The power required is ~15 kW.
  - This produces ~4 mT of O<sub>2</sub> / year (ASSUMES 15% efficiency); Reactor mass is ~60 kg
  - Extraction at 1100 C drops the power requirement to ~11 kW

# Condensation and Collection Module



An additional ~13 kW of cryocooler power to produce 4 mT of O<sub>2</sub> per year

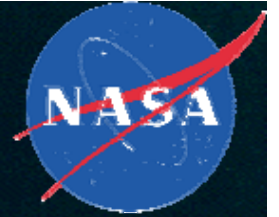


# Conclusions

Changes to the chamber have significantly improved the thermal performance of the chamber and decreased the power requirements.

Faster power ramping greatly decreases the energy requirements

We have built and done preliminary testing on a condensation and collection module.



# Acknowledgments

We would like to thank the following for their contributions to this work:

- Laura Garchar, UNR
- Jason Stein, UW
- Brandon Hall, UM
- Robert Solheim and James Shoji of Pratt & Whitney / Rocketdyne